

**In the Specification:**

Please replace the following amended paragraphs:

**Page 42, paragraph 2, lines 7 to 15 insert the following paragraph:**

A version of the processes described above can be provided in which one of the principal purposes of the process described herein is to maximize recovery of CO<sub>2</sub> for commercial sale. In this case the first operation, which is conducted in the first absorber, rather than allowing a portion of the CO<sub>2</sub> to be deliberately "slipped" into the overhead gas, is designed to recover a major portion of the CO<sub>2</sub> in the rich amine leaving the first absorber. This differs from ~~claim 1—18 or 20—24~~ the arrangement described herein in which CO<sub>2</sub> is recovered but merely as a by-product, which may or may not have commercial value. In ~~claim 19~~ one arrangement described herein, the object is to maximize recovery of CO<sub>2</sub> from the inlet gas for the purpose of producing a marketable CO<sub>2</sub> product.

**Page 43, paragraph 2, lines 2 to 10 insert the following paragraph:**

The rich amine, whether degassed or not, then proceeds to the second absorber, or in the case of a double effect unit, to the second and third absorbers. The rich amine is then contacted with the recycled enriched acid gas and lean amine to produce an overhead product that is essentially pure water saturated CO<sub>2</sub>, ~~as is described in claims 1—18 and 20—24~~. The rich amine leaving the base of the column is then regenerated to produce lean amine plus an enriched acid gas overhead stream, a portion of which is recycled back to the base of the column ~~as described in claims 1—18 and 20—24~~. The balance of this acid gas flows to other processing units, typically a sulphur plant.